

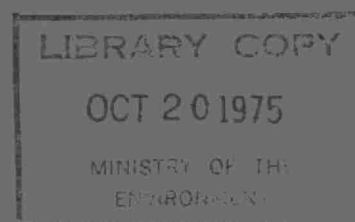
OPERATING SUMMARY

CITY OF

NORTH BAY

WATER POLLUTION CONTROL PLANT

LABORATORY & RESEARCH LIBRARY
MINISTRY OF THE ENVIRONMENT



LAB

1
9
7
4

Copyright Provisions and Restrictions on Copying:

This Ontario Ministry of the Environment work is protected by Crown copyright (unless otherwise indicated), which is held by the Queen's Printer for Ontario. It may be reproduced for non-commercial purposes if credit is given and Crown copyright is acknowledged.

It may not be reproduced, in all or in part, for any commercial purpose except under a licence from the Queen's Printer for Ontario.

For information on reproducing Government of Ontario works, please contact ServiceOntario Publications at copyright@ontario.ca



Ontario

MINISTRY OF THE ENVIRONMENT

MINISTER
Honourable William G. Newman

DEPUTY MINISTER
E. Biggs

ASSISTANT DEPUTY MINISTER
REGIONAL OPERATIONS
J. Barr

REGIONAL OPERATIONS DIVISION

DIRECTOR, NORTHEASTERN REGION
R. Moore

MANAGER, UTILITY OPERATIONS
J. Wesno

NORTH BAY
WATER POLLUTION CONTROL PLANT

operated for

THE CITY OF NORTH BAY

by the

MINISTRY OF THE ENVIRONMENT

1974 ANNUAL OPERATING SUMMARY

prepared by

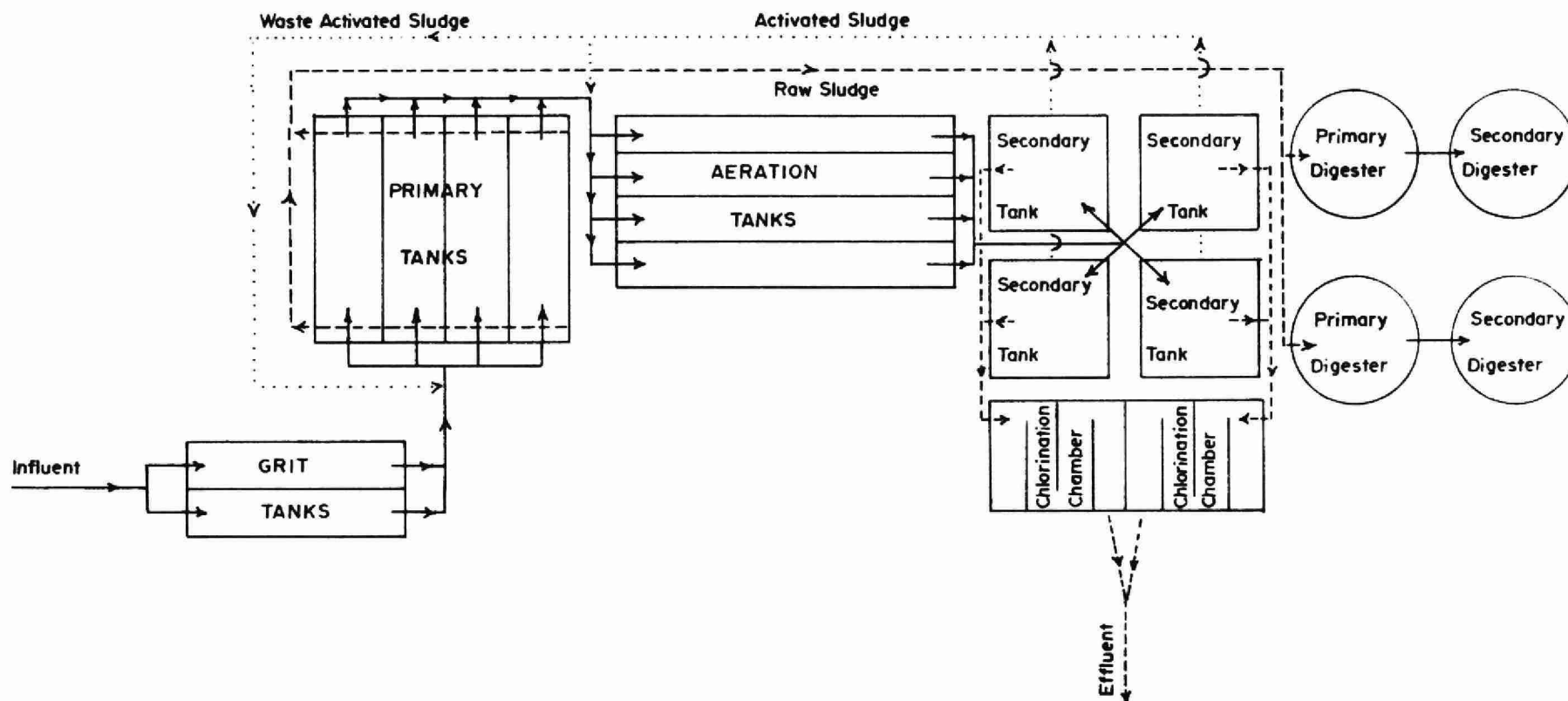
Plant Performance Unit

TECHNICAL SERVICES BRANCH

T. Cross, Director

CONTENTS

Title Page	1
Flow Diagram	4
Design Data	5
'74 Review	6
Project Costs	8
Process Data	10



CITY OF NORTH BAY WPCP

DESIGN DATA

PROJECT: City of North Bay WPCP

PROJECT NUMBER: 2-0010-58

TREATMENT: Activated Sludge

DESIGN FLOW: 8.0 mgd

BOD - Raw Sewage 150 mg/l
- Removal 85%

PRIMARY TREATMENT

GRIT REMOVAL

Type: Aerated grit tanks
Size: two, (each) 48' x 16' x 7.8' awl
(each: 37,380 I.G.)
Retention: (each) 6.8 min

SCREENS

Type: two, Mechanical

SEWAGE LIFT PUMPS

Type: WORTHINGTON
Two, variable-speed
One, constant-speed
Size: (total) 16 mgd

PRIMARY SEDIMENTATION

Type: Four, 90' x 30' x 11'
(741,300 I.G. total)
Retention: 2.2 hr

SECONDARY TREATMENT

AERATION TANKS

Type: Diffused Air, two-pass
Size: Two, 185' x 20' x 12' per pass
(1,108,000 I.G. total)
Retention: 3.3 hr

RETURN SLUDGE PUMPS

Type: WORTHINGTON
Size: Two, 550 gpm

SECONDARY SEDIMENTATION

Type: WALKER RSX
Size: Four, 60' x 60' x 11'
(988,400 I.G. total)
Retention: 3.0 hr
Loading: Surface-550 gal/ft²/day
Weir - 8,000 gal/ft/day

CHLORINATION

Type: four-pass
Size: two, 39' x 7.8' x 6.5' each pass
(98,700 I.G. total)
Retention: 18 min.

OUTFALL

-1,000 ft into Lake Nipissing

SLUDGE HANDLING

DIGESTION SYSTEM

Type: Two-Stage

Primary --

Type: DORR
Size: Two, 65' dia x 22' swd
(911,000 I.G. total)

Secondary --

Size: Two, 65' dia x 22' swd
(911,000 I.G. total)

'74 Review

GENERAL

The North Bay sewage system consists of an 8.0 mgd conventional activated sludge treatment plant, collector sewers and approximately 20 pumping stations, of which the plant, some sewers and 5 pumping stations were financed and constructed by the Ministry of the Environment. A plant staff of 10 operate the Ministry facilities and, in addition, provide emergency electrical service for all the pumping stations.

The plant expansion from 4 mgd to 8 mgd was completed in August 1974. The additional treatment works include new primary and secondary clarifiers, 2 new primary digesters, and facilities for phosphorus removal treatment. Two additional staff members were hired in October 1974 in order to assist in the operation of the expanded plant.

In order to facilitate better sludge handling and reduce sludge haulage costs, additional treatment facilities for dewatering sludge will be provided in 1976. It is proposed that test trials of various type centrifuges for this purpose will be conducted in the summer of 1975. The purchase of the centrifuge will be carried out late in the year with an expected installation date of November, 1976.

OPERATING COSTS

The total operating cost for the project in 1974 was \$211,089. The cost per million gallons of sewage treated during 1974 was approximately \$91.00.

PLANT FLOWS AND CHLORINATION

Flows to the plant increased by approximately 5 percent over the 1973 flows. A total flow of 2,320 million gallons was treated in 1974 which represents an average daily flow of 6.4 million gallons per day, compared with 6.1 million gallons per day in 1973. This represents 80 percent of the plant design capacity of 8.0 mgd. The per capita flow contribution based on a serviced population of 50,000 was 122 gpd.

A total of 87,800 pounds of chlorine was used to disinfect the effluent at an average dosage of 3.8 mg/l.

PLANT EFFICIENCY

The average raw sewage strength was 153 mg/l BOD and 255 mg/l suspended solids. The total loading to the plant in 1974 was 3,549,600 pounds of BOD and 5,916,000 pounds of suspended solids. Of these totals, 2,576,200 pounds of BOD and 4,802,400 pounds of suspended solids were removed by the treatment process, representing a removal efficiency of 73 percent and 81 percent respectively.

The average phosphorus level in the influent for the year was 8.4 mg/l. The average level in the effluent after treatment commenced in August was 1.5 mg/l, which represents a removal efficiency of 82 percent.

AERATION

The average BOD loading of 98 mg/l to the aeration section represented an average organic loading of 35.3 pounds BOD per 1,000 cubic feet of aeration tank capacity. The mixed liquor suspended solids concentration averaged 2,600 mg/l and the F/M ratio averaged 0.28.

SLUDGE DIGESTION AND DISPOSAL

A total of 8.62 million gallons of raw sludge was pumped to the primary digester at an average concentration of 5.3 percent total solids. Digestion and supernatant return reduced the total quantity to 3.35 million gallons at a total solids concentration of 6.3 percent.

A total of 19,902 cubic yards of sludge was removed from the digester by tank truck. Of this total 12,238 cubic yards were spread directly on local farm fields while a further 7664 cubic yards were mixed with sawdust and composted before being spread on fields.

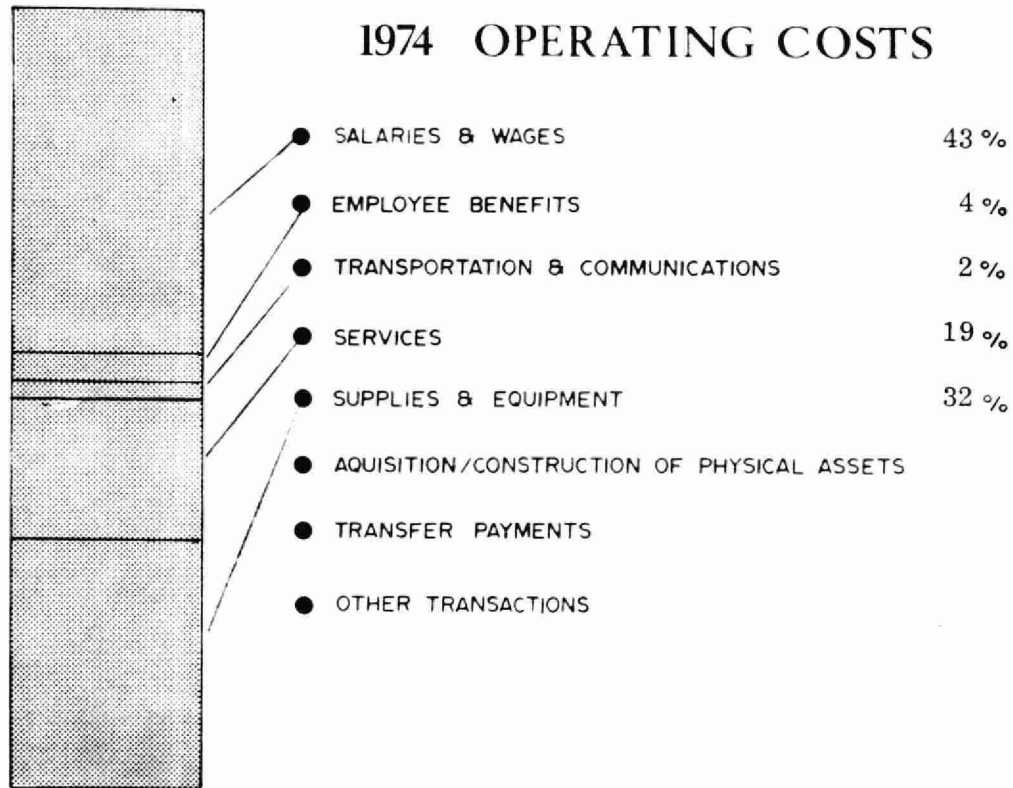
A total of 5582 cubic feet of grit was removed from the plant in 1974. This represents 2.4 cubic feet per million gallons of sewage treated.

CONCLUSIONS

The plant went through a transition period in 1974 in which new treatment facilities were installed and put into service. It is expected that improved plant performance will reflect the plant's new treatment capability.

ANNUAL COSTS

1974 OPERATING COSTS



YEARLY OPERATING COSTS

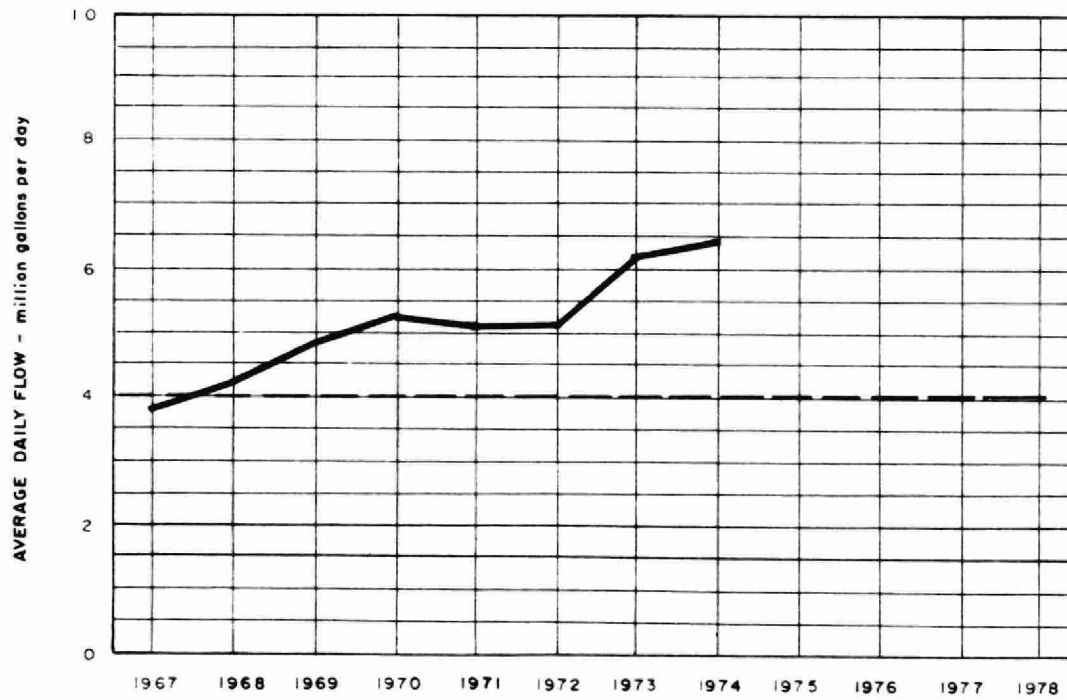
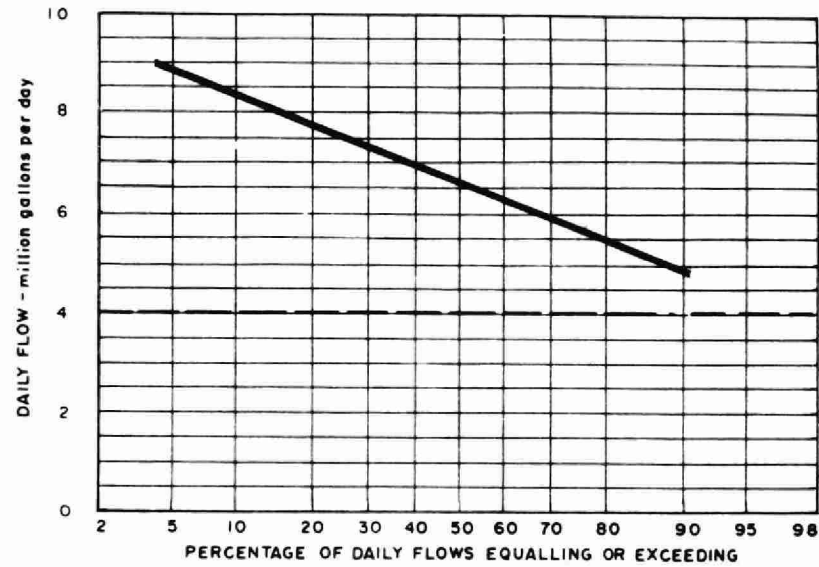
YEAR	SEWAGE TREATED in million gallons	TOTAL OPERATING COSTS	UNIT COSTS	
			\$/M G	¢/lb BOD
1969	1777	121,523	68	7
1970	1957	139,983	72	7
1971	1863	157,917	85	5
1972	1865	184,877	99	9
1973	2218	165,845	74	7
1974	2320 Est.	211,089	91	8

OPERATING EXPENDITURES

Regular Staff	\$ 85,320	\$
Casual (Unclassified) Staff	<u>2,874</u>	
TOTAL SALARIES AND WAGES		<u>88,194</u>
TOTAL EMPLOYEE BENEFITS		<u>8,646</u>
TOTAL TRANSPORTATION AND COMMUNICATIONS		<u>3,967</u>
Insurance	<u>3,490</u>	
Sludge Haulage	<u>32,556</u>	
Repairs and Maintenance	<u>2,722</u>	
Other Services	<u>1,080</u>	
TOTAL SERVICES		<u>39,848</u>
Machinery and Equipment	<u>1,435</u>	
Chemicals	<u>20,257</u>	
Utilities	<u>41,689</u>	
Other Supplies and Equipment	<u>4,854</u>	
TOTAL SUPPLIES AND EQUIPMENT		<u>68,235</u>
TOTAL AQUISITION/CONSTRUCTION OF PHYSICAL ASSETS		<u>-</u>
TOTAL TRANSFER PAYMENTS		<u>-</u>
OTHER TRANSACTIONS		<u>2,199</u>
GRAND TOTAL	GRAND TOTAL	\$ <u>211,089</u>

PROCESS DATA

FLOWS

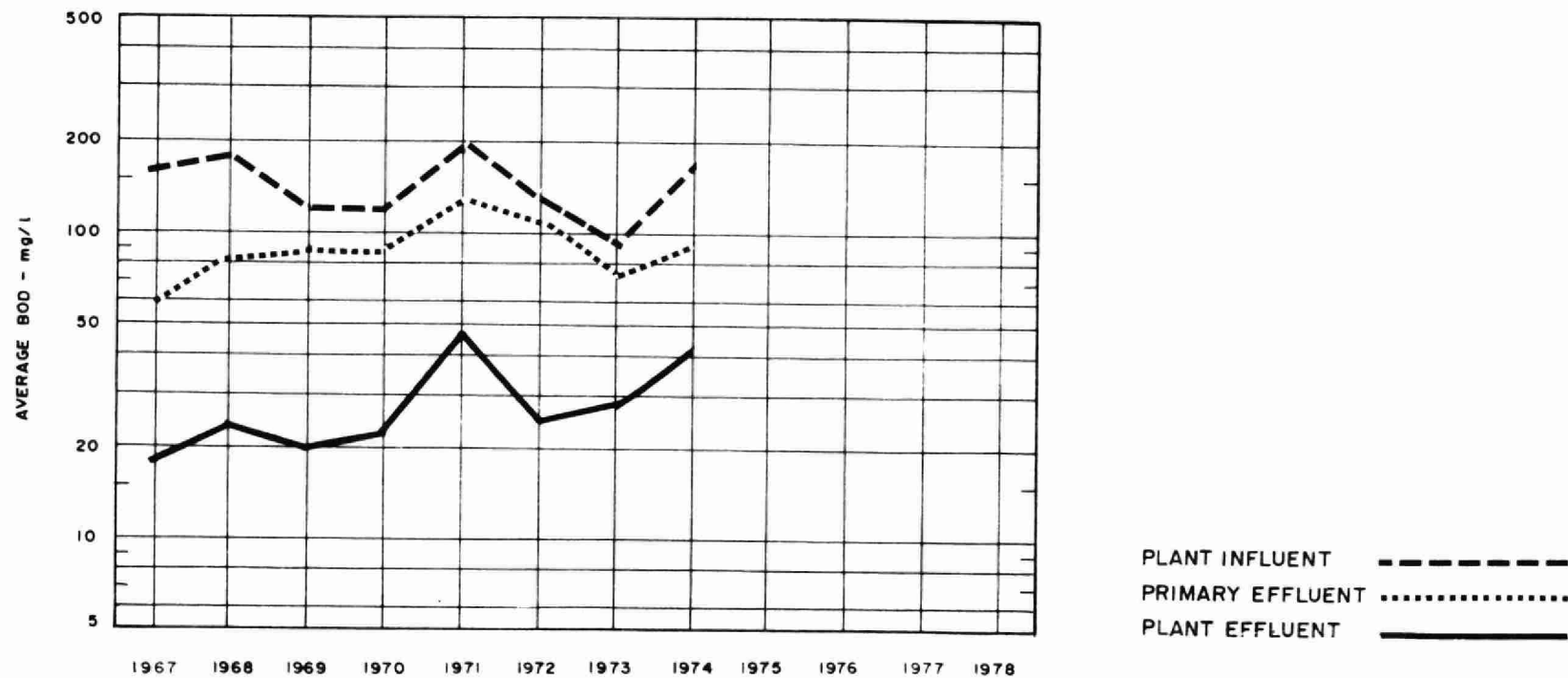
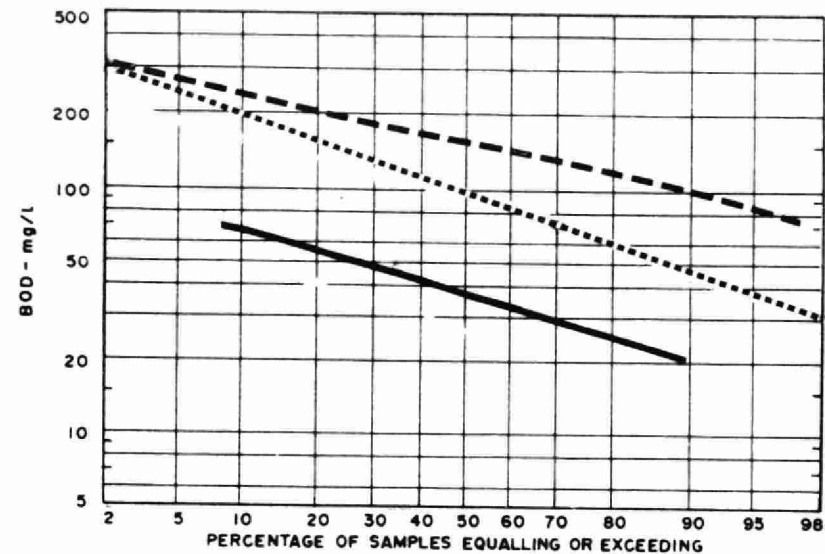


DESIGN CAPACITY - - - - -

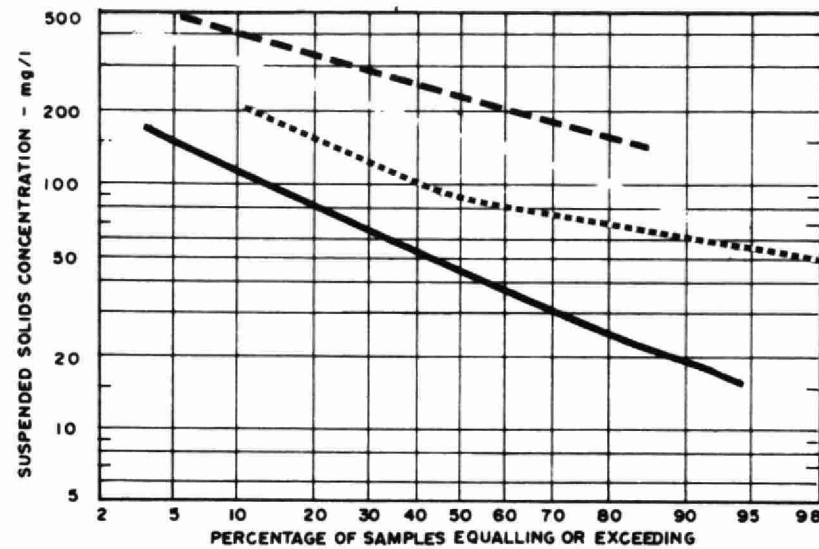
PLANT PERFORMANCE

MONTH	FLOWS			BIOCHEMICAL OXYGEN DEMAND				SUSPENDED SOLIDS				PHOSPHORUS	
	TOTAL FLOW million gallons	AVERAGE DAY mil. gal	MAXIMUM DAY mgd	INFLUENT mg/l	EFFLUENT mg/l	REDUCTION		INFLUENT mg/l	EFFLUENT mg/l	REDUCTION		INFLUENT mg/l P	EFFLUENT mg/l P
						%	10 ⁵ pounds			%	10 ⁵ pounds		
JAN	182	5.9	7.5	183	42	77	2.6	359	46	87	5.7	5.7	3.0
FEB	172	6.1	7.2	149	51	66	1.7	238	55	77	3.1		
MAR	203	6.5	8.2	181	45	75	2.8	191	48	75	2.9		
APR	236	7.9	9.3	154	51	67	2.4	128	67	48	1.4		
MAY	221	7.1	11.0										
JUNE	198	6.6	8.6										
JULY	158	5.1											
AUG	167	5.4		160	22	86	2.3	295	36	88	4.3	16.8	1.0
SEPT	169	5.5	7.9					357	53	85	5.1	8.6	1.5
OCT	202	6.5	7.7	148	30	80	2.4	335	36	89	6.0	6.9	1.7
NOV	247	8.2	13.5	114	37	68	1.9	196	48	76	3.7	5.5	1.0
DEC	165	5.3	6.3	108				193	43	78	2.4	6.1	1.2
TOTAL	2320	-	-	-	-	-		-	-	-		-	-
AVG.		6.4	MAXIMUM 13.5	153	42	73	2.1	255	48	81	5.3	8.4	1.5
No. of Samples	-	-	-	60	46	-	-	140	137	-	-	22	16

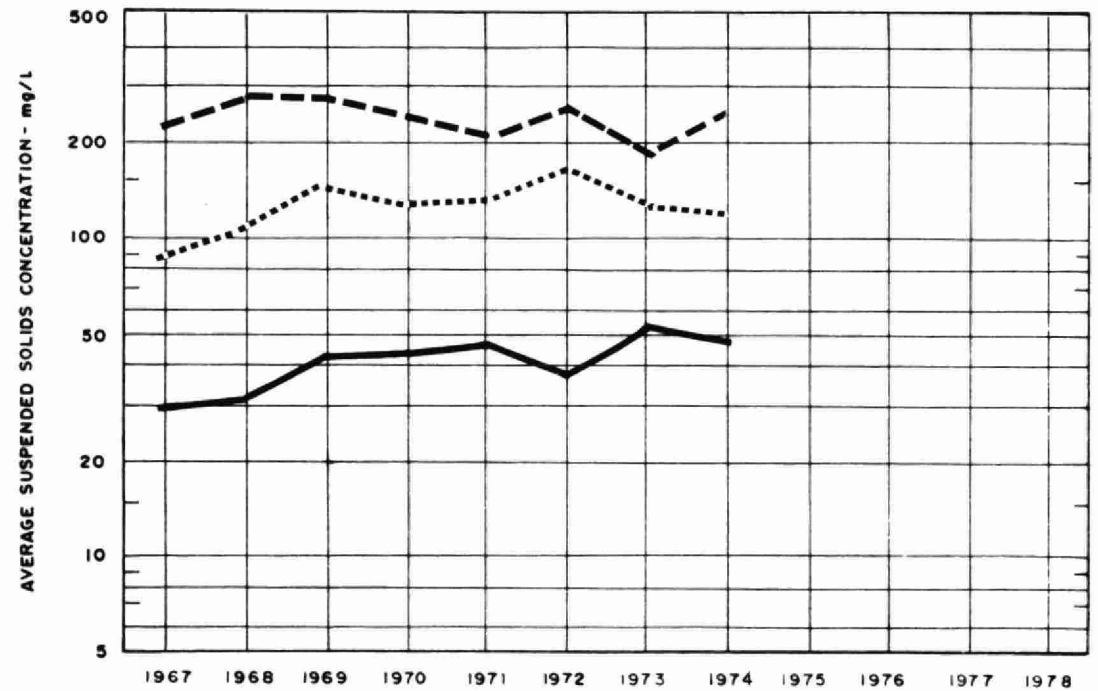
BIOCHEMICAL OXYGEN DEMAND



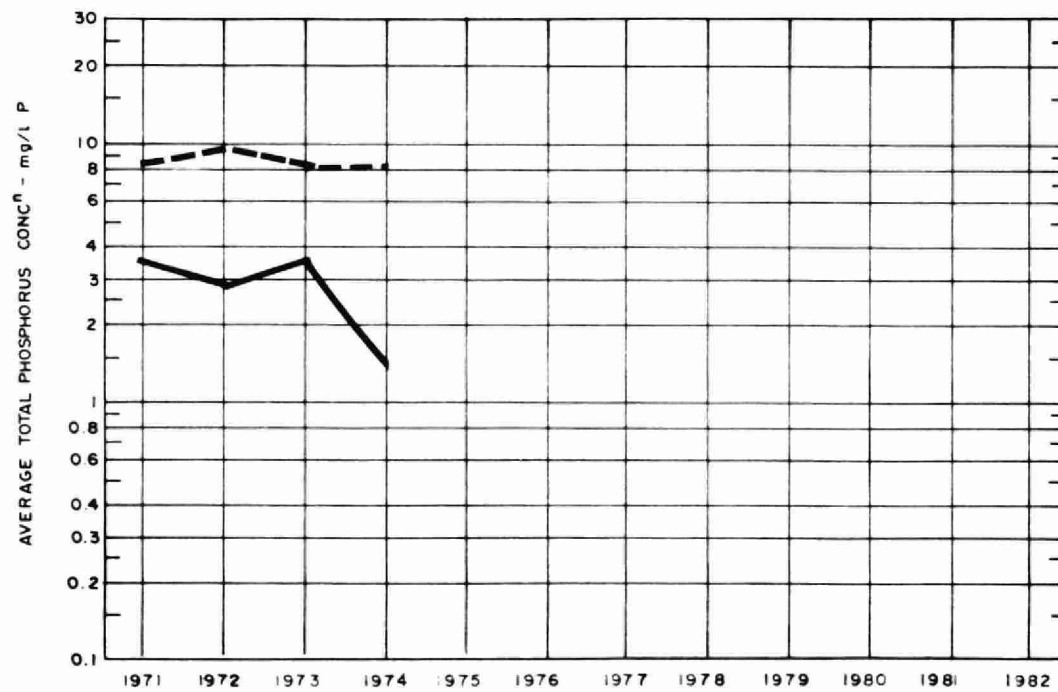
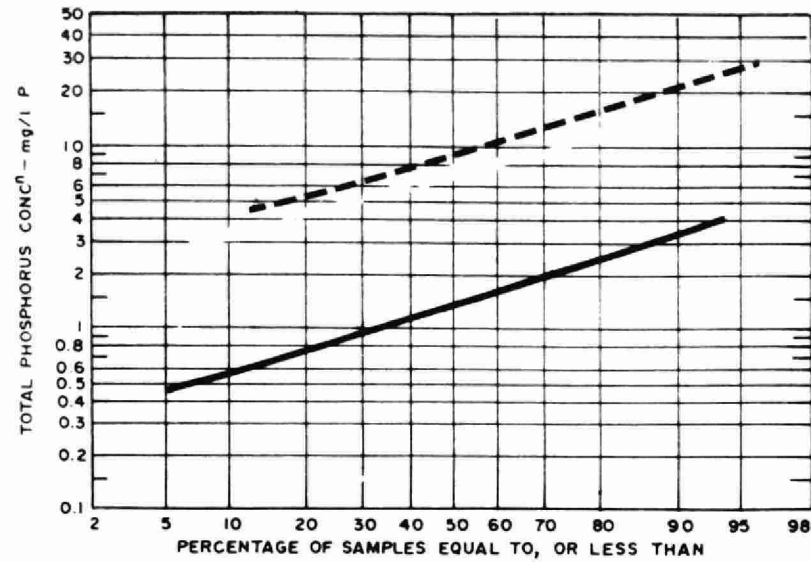
SUSPENDED SOLIDS



PLANT INFLUENT - - - - -
 PRIMARY EFFLUENT
 PLANT EFFLUENT _____



PHOSPHORUS

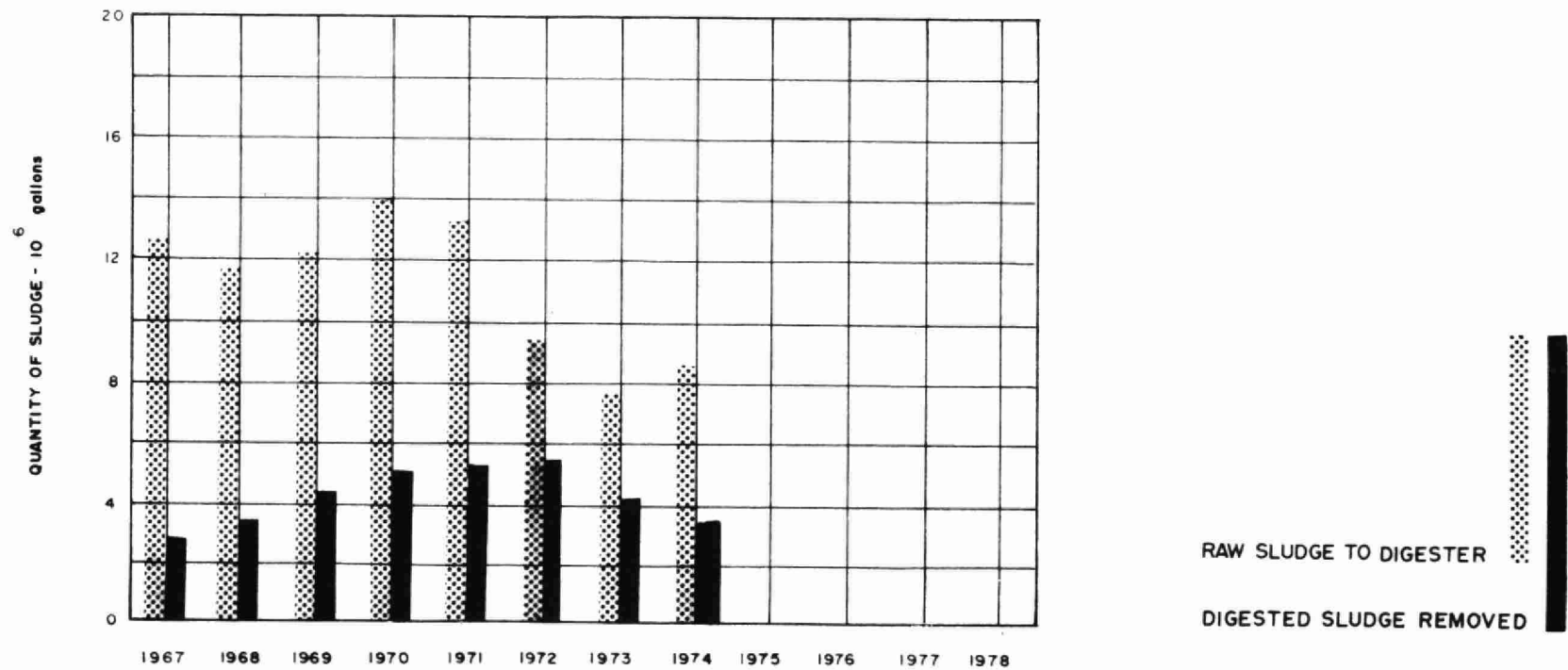
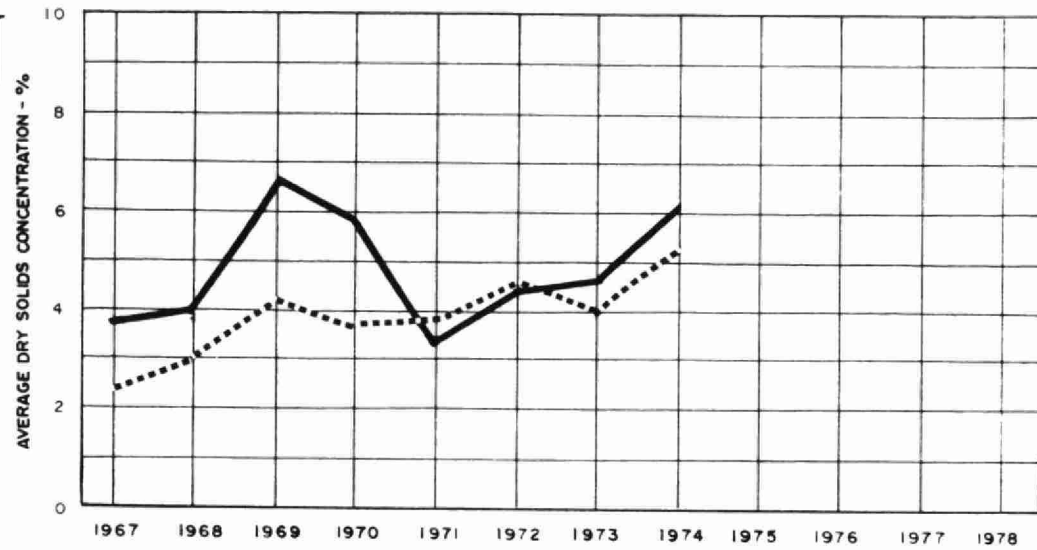


PLANT INFLUENT - - - - -

PLANT EFFLUENT —————

DIGESTION

RAW SLUDGE
DIGESTED SLUDGE ———



TREATMENT DATA

MONTH	GRIT	CHLORINATION		PRIMARY EFFLUENT		AERATION			SLUDGE DIGESTION and DISPOSAL							
	QUANTITY REMOVED cubic feet	CL ₂ USED 10 ³ pounds	AVG. DOSE mg/l	BOD mg/l	SUSPENDED SOLIDS mg/l	MLSS CONC mg/l	F/M day ⁻¹	AIR 1000 ft ³ lb BOD	RAW SLUDGE			DIGESTED SLUDGE			SUPER- NATANT T. S. %	AMOUNT HAULED cubic yards
									QUANTITY 10 ⁶ gallons	TOTAL SOLIDS %	VOL. SOLIDS %	QUANTITY 10 ⁶ gallons	TOTAL SOLIDS %	VOL. SOLIDS %		
JAN	718	9.4	5.1	126	133	1700	.40	1.2	.70	4.6	74	.47	4.8	70	.4	2795
FEB	646	6.8	3.9	136	221	1900	.40	1.1	.36	6.0	72	.28	5.9	63		1693
MAR	836	8.8	4.3	150	171	2000	.44	.8	1.07	4.4	67	.56	3.9	70	.1	3312
APR	1088	9.1	3.8	135	110	2000	.48	.8	.68	5.3	63	.19	9.1	66	.1	1128
MAY	502	8.4	3.8						.70			.15				910
JUNE	926	9.4	4.8						.68			.21				1219
JULY	579	8.1	5.1						.89			.26				1547
AUG	40	5.8	3.4	55	88	1700	.16	3.1	.89	10.1	53	.20	6.5	48	1.3	1201
SEPT		6.6	3.9		102	3400			.54	5.5	61	.35	7.1	57	2.9	2075
OCT		5.0	2.5	80	111	3300	.14	1.9	.88	4.6	67	.58	6.1	62	1.8	3404
NOV	247	6.1	2.8	51	70	2800	.14	1.8	.66	4.0	64					
DEC		4.3	4.5	52	88	4600	.11	2.3	.57	3.6	65	.10				618
TOTAL	5582	87.8	-	-	-	-	-	-	8.62	-	-	3.35	-	-	-	19902
AVG.	2.4 cu. ft/mil gal	7.3	3.8	98	122	2600	.28	1.6	.72	5.3	65	.28	6.2	62	1.1	1659

LABORATORY LIBRARY



96936000119356

Date Due

LAB

PRINTED IN CANADA